

PII: S0017-9310(97)00179-8

## TECHNICAL NOTE

## A critical heat flux correlation for droplet impact cooling at low Weber numbers and various ambient pressures

 W. M. HEALY, P. J. HALVORSON†, J. G. HARTLEY‡ and S. I. ABDEL-KHALIK  
 George W. Woodruff School of Mechanical Engineering, Georgia Institute of Technology, Atlanta,  
 GA 30332-0405, U.S.A.

(Received 20 December 1996 and in final form 7 June 1997)

## INTRODUCTION

Spray cooling has received interest as a technique to dissipate extremely high heat fluxes. Potential applications include the cooling of electronics, lasers, and leading edges of aircraft. Sprays are currently employed in automobile fuel injection systems and quenching of metals in foundries. As a first step in studying spray cooling, single streams of droplets impacting a heated surface have been investigated by a number of authors [1–5]. Although many studies have examined droplet cooling beyond the Leidenfrost temperature, there are numerous practical applications which occur below that point. Recently, Sawyer *et al.* [6] developed a correlation for the critical heat flux (CHF) for a monodispersed stream of droplets; this correlation and its range of applicability are given as follows:

$$\frac{\text{CHF}^*}{\rho_1 h_{fg} V} = 0.1660 We^{-0.4138} St^{0.8906} \quad (1)$$

$$207 < We < 866, \quad 0.007 < St < 0.03.$$

Equation (1) had a 95% confidence level of  $\pm 22\%$  and  $R^2 = 0.964$  for the data upon which it was derived. Table 1 gives a listing of the experimental parameter ranges used. The asterisk on CHF signifies that it is an average heat flux over the initially wetted surface area rather than the entire heated surface area. As noted in [6], such normalization is necessary in order to make the data universally applicable. The droplet was assumed to form a cylindrical film upon impact, and the Kurabayashi–Yang equation [7], equation (2), was used to calculate the diameter of the film.

$$\frac{We}{2} = \frac{3}{2} \beta^2 \left\{ 1 + 3 \frac{We}{Re} \left[ \frac{\mu_1}{\mu_{\text{wall}}} \right]^{0.14} \left[ \beta^2 \ln(\beta) - \frac{\beta^2 - 1}{2} \right] \right\} - 6. \quad (2)$$

Healy *et al.* [8] confirmed that this equation provides accurate predictions of the diameter of the film formed by droplet impact. The correlation of Sawyer *et al.* was checked with an additional data set from Messana [9], who examined the CHF associated with a monodispersed stream of droplets at atmospheric pressure with  $We$  ranging from 245 to 455 and  $St$  ranging from 0.0089 to 0.015. The results showed that the correlation worked well for the new data set with an average absolute error of 9.6%.

As can be seen by the ranges of experimental parameters, equation (1) applies to high values of  $We$ . At these values,

 Table 1. Experimental parameters from Sawyer *et al.* [6] and Halvorson [15]

	Sawyer <i>et al.</i> [6]	Halvorson [15]
$We$	207–866	55–109
$St$	0.007–0.03	0.0019–0.037
$V$ (m s <sup>-1</sup> )	2.4–4.6	1.3
$D$ (mm)	1.5–2.7	2.3–4.0
$f$ (s <sup>-1</sup> )	12–42	1–15
$P$ (atm)	1	0.2–2.0
$\Delta T_{\text{sub}}$ (°C)	75	40–101

droplet impact is expected to result in droplet fragmentation. For droplets impacting a surface heated beyond the Leidenfrost point, it has been found that the droplets break up beyond  $We \approx 70$  [1, 10]. However, a splashing threshold has not been determined for droplets impacting surfaces at low superheats owing to the complex interactions between the spreading droplet and the surface [11]. From pictures of impacting droplets, however, it appears that droplets fragment when  $We > 100$  while lower values of  $We$  generally result in droplets which remain intact [12–14]. Video images from the data of Sawyer *et al.* show that droplet fragmentation occurred for the high  $We$  used in their study.

Recently, a large data base for droplet impact CHF was presented by Halvorson *et al.* [5, 15]. These authors determined CHF by observing the peak in the heat flux vs surface superheat curve as the surface temperature was increased above the saturation point of the fluid. The experimental procedures are described in detail in ref. [5]. Table 1 gives the experimental parameter ranges for these experiments. The data set, which is tabulated in ref. [15], covers a lower range of  $We$  than Sawyer's experiments, and video images of the impact process show no evidence of droplet fragmentation. In addition, ambient pressures for the experiments ranged from 0.2 to 2.0 atmospheres. The results of these experiments were compared to predictions of Sawyer's correlation; Fig. 1 shows a plot of the predicted CHF\* vs the experimental CHF\* for all data points taken at 1 atmosphere. The correlation clearly does not apply in the lower range of  $We$  used in Halvorson's experiments. Furthermore, equation (1) is not able to predict the effects of varying ambient pressure. Distinct trends in the data were observed for different ambient pressures, but the correlation does not include terms to account for the influence of pressure.

The purpose of the present study is to develop a correlation

† Present address: Siemens Nuclear Power Division, Richland, Washington, U.S.A.

‡ Author to whom correspondence should be addressed.

NOMENCLATURE			
$c$	specific heat [kJ (kg K) <sup>-1</sup> ]	$We$	Weber number = $\rho V^2 D / \sigma$ .
$CHF^*$	critical heat flux based on area of spread film [W cm <sup>-2</sup> ]	Greek symbols	
$d$	diameter of fully spread film [mm]	$\beta$	spreading ratio = $d/D$
$D$	diameter of impacting droplet [mm]	$\mu$	viscosity
$f$	frequency [s <sup>-1</sup> ]	$\rho$	density
$h_{fg}$	heat of vaporization [kJ kg <sup>-1</sup> ]	$\sigma$	surface tension.
$P$	pressure [atm]	Subscripts	
$Re$	Reynolds number = $\rho V D / \mu$	atm	atmospheric
$St$	Strouhal number = $f D / V$	f	saturated liquid
$\Delta T_{sub}$	subcooling = saturation temperature minus initial droplet temperature [°C]	g	saturated vapor
$V$	impact velocity [m s <sup>-1</sup> ]	l	liquid at room temperature
		wall	at wall temperature.

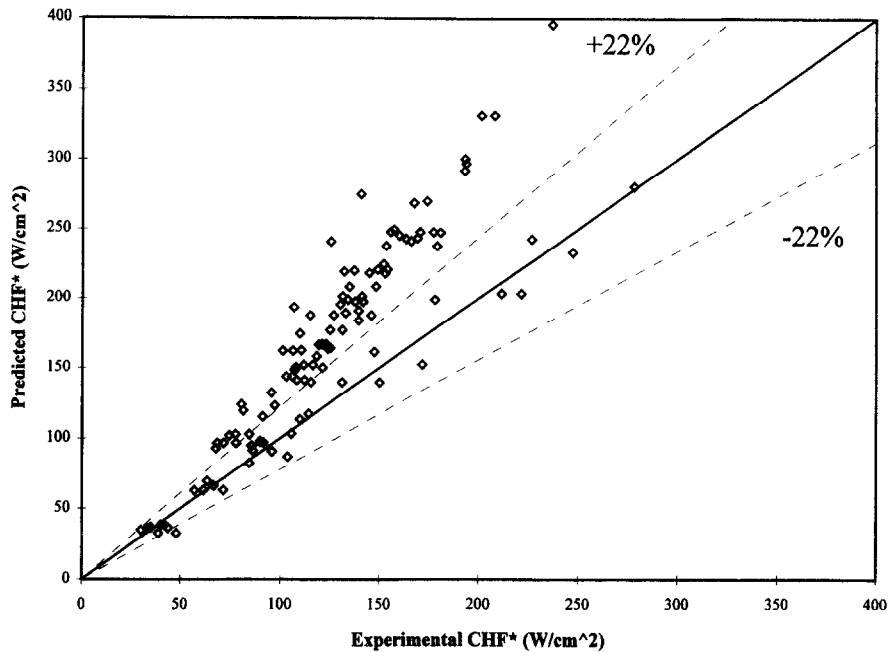


Fig. 1. Comparison between predictions of Sawyer *et al.*'s correlation [6] and experimental data from Halvorson [15] for low Weber numbers at one atmosphere. (Dashed lines represent 95% confidence interval for Sawyer *et al.*'s correlation.)

for CHF\* applicable at low  $We$  and different ambient pressures (i.e. subcoolings) to serve as a companion to the one developed in ref. [6] for high  $We$ .

**CORRELATION DEVELOPMENT**

As a first step in accounting for the influence of pressure, all properties were calculated at the saturation temperature of the liquid. In addition to introducing subcooling as part of an independent parameter in the regression analysis, the newly defined  $We$  and  $Re$  also changed the spreading ratios predicted by equation (2). The effect of subcooling was further accounted for using the approach of Ivey and Morris [16]. This approach involved adding a subcooling correction to the heat of vaporization in the non-dimensional CHF. Even with this correction included, data from experiments at

different pressures were not well correlated. Thus, a pressure ratio ( $P/P_{atm}$ ) was included as an independent parameter in the regression analysis. The resulting correlation is given as equation (3):

$$CHF^* = \rho_l \left[ h_{fg} + 0.1 \left( \frac{\rho_l}{\rho_g} \right)^{3/4} c \Delta T \right] V = 0.146 We^{-0.9816} St^{0.6883} \left( \frac{P}{P_{atm}} \right)^{0.6081} \quad (3)$$

The least-squares fit has an  $R^2$  value of 0.972, and the 95% confidence level is  $\pm 20\%$ .

Figure 2 shows a plot of the predictions of the new cor-

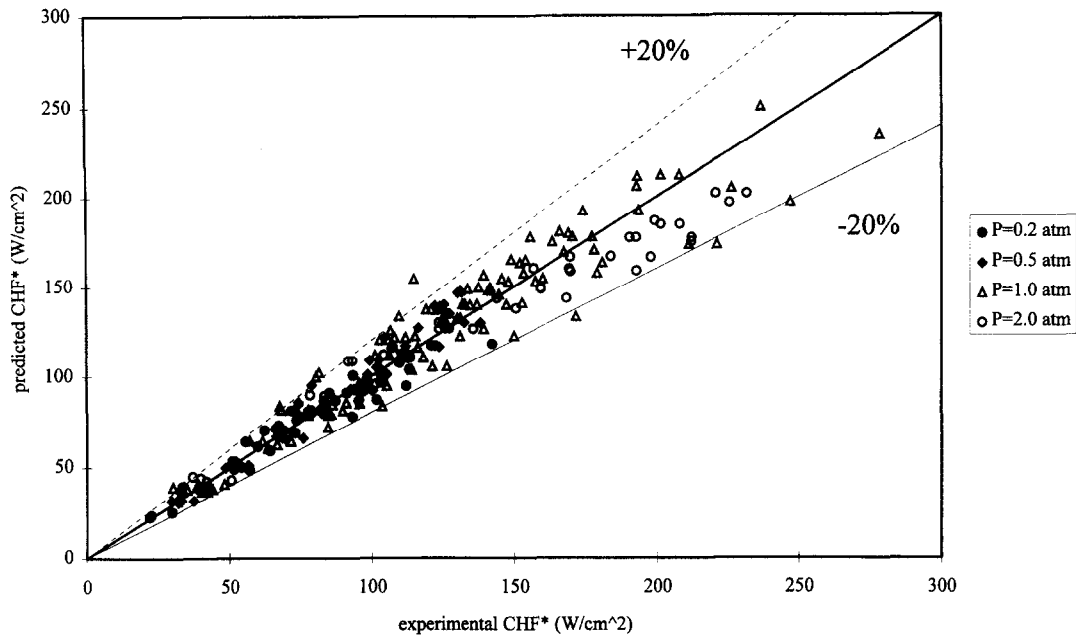


Fig. 2. Comparison between predictions of new correlation and experimental data from Halvorson [15]. (Dashed lines represent 95% confidence interval for new correlation.)

relation versus the experimental value of CHF\* for each data point in Halvorson's data set along with lines that delineate 20% deviations from the experimental values. This new correlation effectively predicts the values of Halvorson's CHF\* for the entire range of  $We$  and  $St$  and for ambient pressures of 0.2–2 atmospheres. Figure 2 also shows that the correlation accounts for the pressure trends in the data. This correlation can be used to estimate the maximum heat transfer rate for a spray consisting of nearly monodispersed drops by multiplying the value of CHF\* by the wetted area of the surface.

**CONCLUSION**

A CHF correlation has been developed for droplet cooling for a range of Weber numbers between 55 and 109 and Strouhal numbers between 0.0019 and 0.037. In this range, it was observed that droplets do not fragment upon impact. The correlation of Sawyer *et al.* [6], developed for higher Weber numbers, did not predict the CHF for this data range well because droplet fragmentation was observed in their experiments and, hence, the heat transfer mechanisms in the two situations are different. For this reason, a separate correlation was developed from that of Sawyer *et al.* [6]. In addition, corrections were made to account for influences of ambient pressure on the CHF resulting in a correlation which is applicable for a variable ambient pressure between 0.2 and 2 atmospheres.

**REFERENCES**

1. Wachters, L. H. J. and Westerling, N. A. J., The heat transfer from a hot wall to impinging water drops in the spheroidal state. *Chemical Engineering Science*, 1966, **21**, 1047–1056.
2. McGinnis, F. K. and Holman, J. P., Individual droplet heat transfer rates for splattering of hot surfaces. *International Journal of Heat and Mass Transfer*, 1969, **12**, 95–108.
3. Pederson, C. O., An experimental study of the dynamic

- behavior and heat transfer characteristics of water droplets impinging upon a heated surface. *International Journal of Heat and Mass Transfer*, 1970, **13**, 369–381.
4. Valenzuela, J. A., Jasinski, T. J. and Drew, B. C., High heat flux evaporative cold plate for space applications. TM-1103, Creare Inc., Hanover, New Hampshire, Phase I Final Report, NASA Contract Nas9-17574, July 1986.
5. Halvorson, P. J., Carson, R. J., Jeter, S. M. and Abdel-Khalik, S. I., Critical heat flux limits for a heated surface impacted by a stream of liquid droplets. *ASME Journal of Heat Transfer*, 1994, **116**, 679–685.
6. Sawyer, M. L., Jeter, S. M. and Abdel-Khalik, S. I., A critical heat flux correlation for droplet impact cooling. *International Journal of Heat and Mass Transfer*, 1997, **40**, 2123–2131.
7. Yang, W. J., Theory on vaporization and combustion of liquid drops of pure substances and binary mixtures on heated surfaces. Technical Report 535, Institute of Space and Aeronautical Science, University of Tokyo, Tokyo, 1975.
8. Healy, W. M., Hartley, J. G. and Abdel-Khalik, S. I., Comparison between theoretical models and experimental data for the spreading of liquid droplets impacting a solid surface. *International Journal of Heat and Mass Transfer*, 1996, **39**, 3079–3082.
9. Messana, M. R., Heat transfer to an accelerated stream of droplets impinging onto a heated surface. Masters thesis, Georgia Institute of Technology, Atlanta, Georgia, 1991.
10. Ueda, T., Enomoto, T. and Kanetsuki, M., Heat transfer characteristics and dynamic behavior of saturated droplets impinging on a heated vertical surface. *Bulletin of the JSME*, 1979, **22**, 724–732.
11. Stow, C. D. and Hadfield, M. G., An experimental investigation of fluid flow resulting from the impact of a water drop with an unyielding dry surface. *Proceedings of the Royal Society of London A*, 1981, **373**, 419–441.
12. Chandra, S. and Avedisian, C. T., On the collision of a droplet with a solid surface. *Proceedings of the Royal Society of London A*, 1991, **432**, 13–41.
13. Qiao, Y. M. and Chandra, S., Evaporative cooling

- enhancement by addition of a surfactant to water drops on a hot surface. *Proceedings of the 1995 National Heat Transfer Conference*, Portland, OR, U.S.A., 1995, pp. 63–71.
14. Zhao, Z. and Poulikakos, D., Heat transfer and fluid dynamics during the collision of a liquid droplet on a substrate—II. Experiments. *International Journal of Heat and Mass Transfer*, 1996, **39**, 2791–2802.
  15. Halvorson, P. J., On the heat transfer characteristics of spray cooling. Ph.D. thesis, Georgia Institute of Technology, Atlanta, GA, 1993.
  16. Ivey, H. J. and Morris, D. J., Critical heat flux of saturation and subcooled pool boiling in water at atmospheric pressure. *Proceedings of the 3rd International Heat Transfer Conference*, Vol. III. Chicago, IL, 1966, pp. 129–142.